Migration and jamming in wide-gap Couette flows of dense suspensions

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- Modeling strategy to capture dynamics of colloids (Modified Stokesian Dynamics)
- Flow in a Widegap Couette cell

Cornstarch



Silica





10 [µm]

0.5 [µm]



"On the dilatancy of media composed of rigid particles in contact" Reynolds 1885

"If in any way the volume be fixed, then all change of shape is prevented."



from wikipedia



"Experiments on a gravity-free dispersion of large solid spheres in a Newtonian fluid under shear" Bagnold 1954

spherical droplets of mixture of paraffin wax and lead stearate ($\sim 1.32 \text{ mm}$)

When shear rate $\dot{\gamma}$ is low, shear stress $\propto \dot{\gamma}$ viscous effect of solvent When shear rate $\dot{\gamma}$ is high, shear stress $\propto \dot{\gamma}^2$ particle inertia



Hydrodynamic theory **Einstein 1906** $\eta = \eta_0(1 + 2.5\phi)$ for $\phi \ll 1$

Batchelor & Green 1972

 $\eta \approx \eta_0 (1 + 2.5\phi + 6.9\phi^2)$ \uparrow \uparrow two-body problem one-body problem



from wikipedia



from http://www.che.caltech.edu

Hydrodynamic simulation

Stokesian Dynamics Brady & Bossis 1985

6N-dimensional overdamped Langevin eq.

 $F_{\rm H} + F_{\rm B} = 0$

 $F_{\rm H} = -\boldsymbol{R} \cdot (\boldsymbol{U} - \boldsymbol{u}) + \boldsymbol{R}' : \boldsymbol{D}$ $\boldsymbol{u}(\boldsymbol{r}) = \nabla \boldsymbol{u} \cdot \boldsymbol{r} = \boldsymbol{D} \cdot \boldsymbol{r} + (\boldsymbol{\omega}/2) \times \boldsymbol{r}$





Mechanical properties of fluid materials

Liquid Newtonian

$$\boldsymbol{\sigma} = -p\boldsymbol{I} + 2\eta\boldsymbol{D}$$
$$\boldsymbol{D} \equiv \frac{1}{2} \left(\nabla \boldsymbol{u}[\boldsymbol{r}(t), t] + \nabla \boldsymbol{u}^{\mathrm{T}}[\boldsymbol{r}(t), t] \right)$$

Molcular dynamics



mean free path² $\sim 10^{-11}$ [s] velocity

Suspensions Non-Newtonian



Stokesian dynamics



 $\frac{\text{radius}^2}{\text{diffusion constant}} \sim 1 \,[\text{s}]$





microstructure





Zero-Reynolds number hydrodynamics

Navier-Stokes equations (non-linear)

$$Re\left\{\frac{\partial \vec{u}}{\partial t} + \left(\vec{u} \cdot \nabla\right)\vec{u}\right\} = -\nabla p + \nabla^{2}\vec{u}$$
$$Re \equiv \frac{\rho_{0}a^{2}\dot{\gamma}}{\eta_{0}} \to 0$$

Stokes equations (linear)

$$\overrightarrow{0} = -\nabla p + \nabla^2 \overrightarrow{u}$$

Hydrodynamic interactions

(6 N dimension)

$$F_{\rm H} = -\boldsymbol{R} \cdot (\boldsymbol{U} - \boldsymbol{u}) + \boldsymbol{R}' : \boldsymbol{D}$$

$$\boldsymbol{u}(\boldsymbol{r}) = \nabla \boldsymbol{u} \cdot \boldsymbol{r} = \boldsymbol{D} \cdot \boldsymbol{r} + (\boldsymbol{\omega}/2) \times \boldsymbol{r}$$

cf. Stokes drag $R = 6\pi\eta_0 aI$



Newtonian dynamics vs. Overdamped dynamics



 $\rho = 1000 \, [\text{kg/m}^3]$

$$0 \rightarrow m \frac{dU}{dt} = -6\pi\eta_0 aU$$

$$U(0) = U_0$$

$$U(\Delta t) = 0$$

$$\Delta t \gg \tau$$

$$U(t)$$

$$0.8$$

$$0.6$$

$$0.4$$

$$0.2$$

$$1 - 2$$

$$3 - 4$$

$$t/\tau$$

cf. time-scale of shear flow

 $\tau_{\rm shear} = 1/\dot{\gamma}$

Purely hydrodynamic suspensions

force balance eq. $F_{\rm H} = 0$

hydrodynamic interaction $F_{\rm H} = - R \cdot (U - u) + R' : D$

Perfect reversibility, if lubrication layers can remain.





shear reversal demo

Singularity of non-Brownian simulation



Minimum gap

Regularize the singularity

lubrication force

$$\boldsymbol{F}_{\text{lub}} = -\frac{3\pi\eta_0 a^2}{2h} (\boldsymbol{U}^i - \boldsymbol{U}^j) \cdot \boldsymbol{nn}$$

$$\frac{1}{h} \rightarrow \begin{cases} \frac{1}{h+\delta} & h > 0\\ \frac{1}{\delta} & h \le 0 \end{cases} \qquad \delta = 10^{-3} \delta$$



Particle contacts are no longer forbidden!!



$$F_{\rm H} + F_{\rm C} = 0$$

$$F_{\rm H} = -\operatorname{R} \cdot (U - u) + \operatorname{R}' : \operatorname{D}$$





Contact deformation of Silica

$$F_n = k_n (2a - r)^{3/2}$$
$$k_n = \frac{4}{3}E\sqrt{a}$$



a large shear stress

 $\sigma_{xy} = 10^3 \, [Pa]$



typical force

 $F_n \sim \sigma_{xy} \times (2a)^2 = 4 \times 10^{-9} \text{ [N]}$

overlap $\frac{2a-a}{a}$

$$\frac{2a-r}{a} \approx 10^{-5}$$

This level of stiffness is very difficult in simulation!!

With and without hydrodynamic lubrication



Hydrodynamic vs contact force contributions



Force-chain network in 2D simulation repulsive $\bar{F}_{ij} \equiv -\vec{F}^{(ij)} \cdot \vec{n}_{ij}$ attractive $\phi_{\rm area} = 0.8 \qquad \mu = 0.5$ $\phi_{area} = 0.7$ $\mu = 0.5$

Angular dependence of normal force



Only hydrodynamics forces are able to be attractive

$$\phi_{\text{area}} = 0.7 \quad \mu = 0.5$$

contribution to shear stress σ_{xy}

$$\phi_{\text{area}} = 0.8 \qquad \mu = 0.5$$

contribution to shear stress σ_{xy}

With and without contact friction

with rolling friction

2D demo for an extreme contact model

no slide and rolling as long as pushing

How do shear flows bring Brownian hard spheres to non-equilibrium states?

Stokesian Dynamics was introduced to tackle this problem 6N-dimensional overdamped Langevin eq.

$$F_{\rm H} + F_{\rm B} = \mathbf{0}$$
$$u(r) = \nabla u \cdot r = \mathsf{D} \cdot r + (\omega/2) \times r$$

hydrodynamic force $F_{\rm H} = - R \cdot (U - u) + R' : D$ Brownian force $\langle F_{\rm B} \rangle = 0$, $\langle F_{\rm B}(t_1)F_{\rm B}(t_2) \rangle = 2k_{\rm B}TR\delta(t_1 - t_2)$

Modified Stokesian Dynamics

Step 1: Remove lubrication singularity

$$\downarrow F_{\rm H} + F_{\rm B} + F_{\rm C} = 0$$

Step 2: Introduce a contact-force model

Contacts in sheared Brownian motions Pe = 1Pe = 100

Péclet number: Pe $\equiv \frac{6\pi\eta_0 a^3\dot{\gamma}}{k_{\rm B}T}$

Experimental data $a = 125 \,\mathrm{nm}$ $a = 260 \, \text{nm}$ $a = 225 \,\mathrm{nm}$ $\eta_0 = 0.049 \,\mathrm{Pa\,s}$ $\eta_0 = 0.001 \, \text{Pa s}$ $\eta_0 = 0.05 \, \text{Pa s}$ $\phi = 0.5$ $\phi = 0.52$ 1000 1000 1000 $0 \mu/\mu$ $\phi = 0.52$ 100 100 10 10 10 0.2 0.3 0.091000 0.001 1000 0.001 1000 0.001 0.100 10 0.100 10 0.100 10 Pe Pe Pe Egres 2005 Cwalina 2014 Laun 1984 Prof. Wagner's group

To match experimental data

Stokesian Dynamic + DEM

- Introduction a bit of history
- Modeling strategy to capture dynamics of colloids (Modified Stokesian Dynamics)

Flow in a Widegap Couette cell

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Suspensions Non-Newtonian

Stokesian dynamics

diffusion constant

Force-balance dynamics with fixed particles

• Velocities of mobile particles to be solved: $\boldsymbol{U}^{m} = (\boldsymbol{U}^{(1)}, \dots, \boldsymbol{U}^{(n)})$ • Velocities of fixed particles: $\boldsymbol{U}^{f} = (\boldsymbol{U}^{(n+1)}, \dots, \boldsymbol{F}^{(n+m)})$

step1 $\boldsymbol{U}^{m} = (\boldsymbol{R}_{FU}^{mm})^{-1} \left(\boldsymbol{F}_{P}^{m} - \boldsymbol{R}_{FU}^{mf} \boldsymbol{U}^{f} \right)$ dynamicsstep2 $\boldsymbol{F}_{rct}^{f} = \boldsymbol{R}_{FU}^{fm} \boldsymbol{U}^{m} + \boldsymbol{R}_{FU}^{ff} \boldsymbol{U}^{f} - \boldsymbol{F}_{P}^{f}$ used in rheology

Monolayer simulation for wide-gap Couette cells

Summary

Simulation models for colloidal suspensions are very different from MD simulations. (Particles are not points)

We introduced a Modified Stokesian Dynamics simulation.

- A realistic choice to avoid lubrication singularity
- Various possibilities for contact interaction between colloids
- Additional force is essential for rate-dependence

Although we now know rheology of dense suspensions well, we know little about fluid mechanics of dense suspensions